This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Currently Amended): A method of ~~for manufacture of~~ preparing a granulate containing at least one polyvinylacetal, said method comprising converting a polyvinylacetal-containing composition into a molten state by heating to 100 to 340 °C in a single or double screw extruder having a main inlet and at least one side stream inlet, wherein at least one part of the polyvinylacetal-containing composition is introduced into said screw extruder via said at least one side stream inlet, and granulating the resultant material to the desired particle sizes.

2. (Cancelled):

3. (Cancelled):

4. (Previously Presented): The method in accordance with Claim 1, wherein granulating of the resultant material is performed by hot pelletization.

5. (Previously Presented): The method in accordance with Claim 1, wherein during conversion to the molten state a foaming agent is added to the polyvinylacetal-containing composition.

6. (Cancelled):

7. (Currently Amended): The method in accordance with claim 1 ~~6~~, wherein at least 90 wt% of the polyvinylacetal-containing composition is introduced into said screw extruder via at least one side stream inlet.

8. (Currently Amended): The method in accordance with claim 1 ~~6~~, wherein said at least one side stream inlet is cooled by cooling means.

9. (Currently Amended): The method in accordance with Claim 1, wherein ~~characterized in that~~ the region of the extruder from the main inlet up to a length equal to at least 15*L/D times the diameter of the screw is cooled, wherein L represents the length of the screw and D represents the diameter of the screw.

10. (Previously Presented): The method in accordance with Claim 1, wherein at least one of the extruder screws is cooled.

11. (Currently Amended): The method in accordance with claim 10, wherein ~~characterized in that~~ the screw is cooled over the range of the extruder from the main inlet up to a length equal to at least 10*L/D, wherein L represents the length of the screw and D represents the diameter of the screw.

12. (Previously Presented): The method in accordance with Claim 8, the temperature of the cooling means used to cool said at least one side stream inlet is less than or equal to the glass transition temperature of the polyvinylacetal-containing composition.

13. (Previously Presented): The method in accordance with Claim 1, wherein the temperature in feeding of the polyvinylacetal-containing composition into the molten state is changed.

14. (Previously Presented): The method in accordance with claim 9, wherein, during the conversion of the polyvinylacetal-containing composition into the molten state, the temperature in said screw extruder is increased.

15. (Previously Presented): The method in accordance with Claim 1, wherein gaseous compounds, which arise upon conversion of the polyvinylacetal-containing composition into the molten state, are removed from the composition.

16. (Previously Presented): The method in accordance with claim 15, wherein a part of the gaseous compounds is removed via the main entry port of the screw extruder.

17. (Currently Amended): The method in accordance with Claim 1 ~~6~~, wherein the side stream input of said at least one part of the polyvinylacetal-containing composition takes place by means of a dosing device with one or two screw-conveyors.

18. (Previously Presented): The method in accordance with Claim 1 ~~6~~, wherein the diameter of the extruder screw or screws is larger than the diameter of the one or two screw-conveyors of the dosing device.

19. (Previously Presented): The method in accordance with Claim 18, wherein the ratio of the screw diameter of the extruder to the screw diameter of the side stream dosing device lies in the range from 1.1:1 to 10:1.

20. (Currently Amended): The method in accordance with Claim 1 ~~6~~, wherein the temperature in the region of the side stream dosing device is less than or equal to the glass transition temperature of the polyvinylacetal-containing composition.

21. (Previously Presented): The method in accordance with Claim 1, wherein the polyvinylacetal-containing has a glass transition temperature greater than or equal to 0 °C.

22. (Previously Presented): The method in accordance with Claim 1, wherein the polyvinylacetal-containing composition comprises 95 wt% polyvinylacetal.

23. (Currently Amended): The method in accordance with Claim 1, wherein the polyvinylacetal-containing composition contains external softener, and the amount of external softener is at the most 2 wt% ~~external softener~~.

24. (Withdrawn): The granulate obtainable according to a method in accordance with Claim 1.

25. (Previously Presented): A method according to claim 1, wherein the resultant

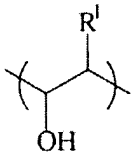
granulate produced has a bulk density, in accordance with Standard 543, of greater than 350 g/l.

26. (Previously Presented): A method according to claim 1, wherein the resultant granulate has a d_{50}/d_{90} value greater than 0.70.

27. (Previously Presented): A method according to claim 1, wherein the resultant granulate contains at least 50.0 wt% of at least one polyvinylacetal, with respect to the total weight.

28. (Previously Presented): A method according to claim 27, wherein in the resultant granulate the polyvinylacetal is obtainable through reaction of at least a polymer (A) with at least a compound (B), wherein the polymer (A) contains

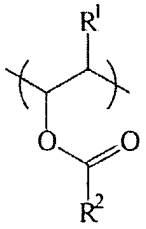
1.0 to 100.0 wt% structural units of formula (1)



(1)

wherein R^1 is hydrogen or methyl,

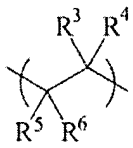
b.) 0 to 99.0 wt% structural units of formula (2)



(2)

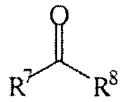
wherein R^2 is hydrogen or an alkyl group with 1 to 6 carbon atoms,

c.} 0 to 70.0 wt% structural units of formula (3)



(3)

wherein R^3, R^4, R^5 and R^6, are, in each case independently of each other, groups with a molecular weight in the range from 1 to 500 g/mol, and the compound (B) satisfies formula (4),



(4)

wherein R^7 and R^8, in each case independently of each other, are hydrogen, COOH, COOM, an alkyl group with 6 to 12 carbon atoms, or an aryl group 6 to 12 carbon atoms, and M is a metal cation or if applicable an alkylated ammonium cation.

29. (Previously Presented): A method according to claim 1, wherein the resultant granulate contains other additives.

30. (Previously Presented): A method according to claim 1, wherein the resultant granulate contains fiber-strengthening materials.

31. (Previously Presented): A method according to claim 30, wherein the resultant granulate contains short glass fibers, long glass fibers, aramid fibers and/or carbon fibers as fiber strengthening material.

32. (Withdrawn): The granulate in accordance with Claim 24, characterized in that one solution prepared from the obtained granulate has a yellow value less than or equal to 3.

33. (Previously Presented): A method according to claim 28, wherein the polyvinylacetal has a glass transition temperature greater than or equal to 0 °C.

34. (Withdrawn): In a method of preparing a polyvinylacetal solution, the improvement wherein said polyvinylacetal solution is prepared from granulates produced according to the method of claim 1.

35. (Withdrawn): In a method of preparing a film, the improvement wherein said film is prepared from granulates produced according to the method of claim 1.

36. (Withdrawn): In a method of preparing laminated safety glasses using a polyvinylacetal film, the improvement wherein said film is prepared from granulates produced according to the method of claim 1.

37. (Withdrawn): The use of a granulate according to Claim 24 as binding agent.

38. (Previously Presented): The method in accordance with Claim 1, wherein granulating of the resultant material is performed by cold pelletization.

39. (Previously Presented): The method in accordance with Claim 1, wherein said polyvinylacetal-containing composition is converted into the molten state by heating to 130 to 200 °C in said single or double screw extruder.

40. (Previously Presented): The method in accordance with Claim 1, wherein the resultant granules have a d_{10}/d_{100} value that is greater than 0.2, a d_{50}/d_{100} value that is greater than 0.2, and a d_{50}/d_{90} value that is greater than 0.70.

41. (Previously Presented): The method in accordance with Claim 1, wherein the resultant granules have a d_{10}/d_{100} value that is greater than 0.99, a d_{50}/d_{100} value that is greater than 0.99, and a d_{50}/d_{90} value that is greater than 0.99.

42. (Previously Presented): A method according to claim 1, wherein the resultant granulate has a bulk density, in accordance with Standard 543, of greater than 550 g/l.

43. (Previously Presented): A method according to claim 1, wherein the resultant granulate has a bulk density, in accordance with Standard 543, of greater than 600 g/l.

44. (Previously Presented): A method according to claim 1, wherein the resultant granulate has a bulk density, in accordance with Standard 543, of greater than 650 g/l.

45. (Previously Presented): A method according to claim 1, wherein the resultant granulate has a bulk density, in accordance with Standard 543, of greater than 700 g/l.

46. (New): A method according to claim 1, wherein at least 70 wt% of the total weight of the polyvinylacetal-containing composition is introduced into said screw extruder via said at least one side stream inlet, said main entry remains open through which volatile components can escape.